

ADSORPTION OF SULFONE COMPOUNDS IN THE OXIDATIVE DESULFURIZATION PROCESS USING ACTIVATED CLAY: EQUILIBRIUM AND KINETIC STUDY

LU M.C.¹, SAPITAN J.F.², WAN M.W.¹ and BALLESTEROS F.C.JR.²

¹ Department of Environmental Resources Management, Chia-Nan University of Pharmacy and Science, Tainan 71710, Taiwan, ²Environmental Engineering Graduate Program, University of Philippines-Diliman, Quezon City, Philippines 1800 E-mail: mmclu@mail.cnu.edu.tw

The inevitable and incessant combustion of diesel fuel has been proven to continuously produce more particulates and other harmful pollutants. Studies showed that combustion of diesel fuel produces precursors of sulfuric acid which causes ecosystem destruction such as acidification of bodies of water and destruction of crops and sulphate which is the main component of harmful respirable particles in the atmosphere (Alhamed and Bamufleh, 2008; Collins, 1997; Duarte *et al.*, 2011). In order to alleviate these negative impacts, environmental laws on sulfur content of diesel fuel were enacted all over the world. In most developed countries like United States, Japan and Europe, the maximum sulfur concentration in highway diesel was limited to 15 ppm(Anisimov and Tarakanova, 2009; Babich and Moulijn, 2002; Bakar *et al.*, 2012; Stanislaus *et al.*, 2010; Sundararaman and Song 2010).

In diesel, the primary sulfur compounds that need to be removed in reducing its sulfur content are comprised of benzothiophene (BT), dibenzothiophene (DBT), and their alkyl derivatives (Anisimov and Tarakanova, 2009). Over the convention hydrodesulfuzation (HDS), oxidative desulfurization (ODS) was studied to be more cost-effective and more efficient in oxidizing the refractory compounds, predominantly, 4, 6-disubstituted dibenzothiophenes (DBT) (Alhamed and Bamufleh, 2008; Chica *et al.*, 2006; Feng, 2009; Gatan *et al.*, 2004; Liotta and Han, 2003; Wang *et al.*, 2003; Zhang *et al.*, 2009; Zhou *et al.*, 2009). Generally, there are two main reactions involved in ODS process. First, the divalent sulphur atom of the organic sulphur compounds undergoes electrophilic addition of oxygen atoms from the catalyst to form the sulfone (Chica *et al.*, 2006). Then, the formed sulfone having different chemical and physical properties from those of fuel oil hydrocarbons is removed through conventional separation techniques such as distillation, solvent extraction, adsorption, and decomposition (Alhamed and Bamufleh, 2008). This study is focused on the removal of sulfone from oxidized diesel using activated clay through adsorption.

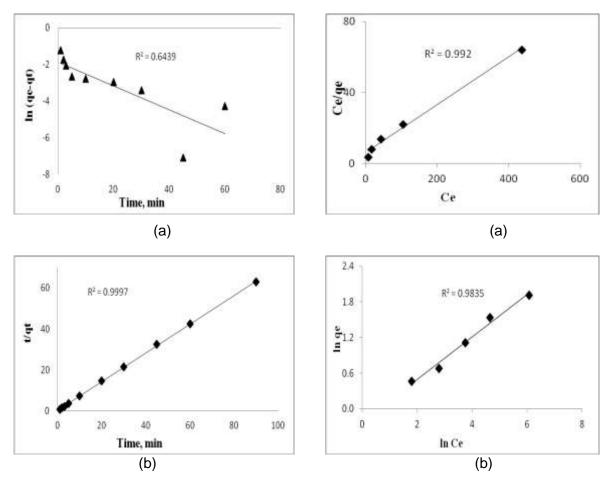
In this study, oxidation of diesel was done using a high-shear mixer (IKA Ultra Turrax T25 digital) set at 15000 rpm for 30 minutes. Diesel fuel (1109.3 ppm S) was mixed with tetraoctylammonium bromide, TOAB (98%, Merck) and hydrogen peroxide, H2O2 (50 %, Merck) containing phosphotungstic acid, HPW (98%, Merck). After mixing, the oil phase which is the oxidized diesel was decanted from the mixture. To further remove the sulfur containing compounds found in the oxidized diesel, it was processed in a batch adsorption method. Activated clay was used as an adsorbent. The sulfur content of diesel in every stage of the oxidative desulfurization process was analyzed using total sulfur analyzer, SLFA 2100 Horiba. The data resulting from this experiment was used for the evaluation of adsorption isotherm and kinetic study.

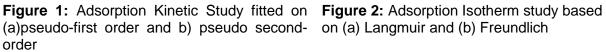
The controlling mechanism of the adsorption process was verified through the different adsorption kinetics models (Chen *et al.*, 2012).. In this study, experimental data were fitted to pseudo-first and pseudo-second order rate reaction as shown in figure 1.

The correlation coefficients R² from resulting graphs were compared to verify the acceptability of the models. Based on figure 1, pseudo-second order model has a high R2 value (0.997) compared with pseudo-first order R2 value (0.6439). This indicates that adsorption of sulfone

onto activated clay is well explained by pseudo-second order rate model. As pseudo-second order rate model fitted well the adsorption of sulfone compounds onto activated clay, it means chemisorption is the rate-limiting step. Therefore, the adsorption process is dominated by physical adsorption. Physical adsorption describes that the intermolecular attraction between sulfone compounds and activated clay particles is governed by van der Waals force.

In addition, comparing the correlation coefficient of the two isotherms, Langmuir better represents the adsorption of sulfone better. Isotherms describe the interactive behaviour of adsorbate and adsorbent. Therefore, the adsorbate forms a monolayer on the surface of the adsorbent.





Keywords: Oxidative Desulfurization, Sulfone, Adsorption, Activated Clay, Diesel

REFERENCES

- 1. Alhamed, Y., Bamufleh, H. (2008), Sulfur removal from model diesel using granular activated carbon from dates' stone activated by ZnCl2. Fuel 88 87-94.
- 2. Anisimov A.V., Tarakanova A.V. (2009), Oxidative Desulfurization of Hydrocarbon Raw Materials. Russian Journal of General Chemistry, 2009, Vol. 79, No. 6, pp. 1264–1273. ISSN 1070-3632.
- 3. Babich, I., Moulijn, J. (2002), Science and Technology of Novel Processes for deep desulfurization of oil refinery streams: A review. Fuel, 82 607-631.
- 4. Bakar, W. A., Ali, R., Kadir, A. A., Mokhtar, W. N. (2012), Effect of transition metal oxides catalysts on oxidative desulfurization of model diesel. Fuel Processing Technology 101, 78–84.

- 5. Chen, F., Zhou, C., Li, G., Peng, F. (2012), Thermodynamics and kinetics of glyphosate adsorption on resin D301. Arabian Journal of Chemistry, http://dx.doi.org/10.1016/j.arabjc.2012.04.014.
- 6. Chica, A., Corma, A., Dómine, M. (2006), Catalytic oxidative desulfurization (ODS) of diesel fuel on a continuous fixed-bed reactor. Journal of Catalysis 242, 299–308. www.elsevier.com/locate/jcat.
- 7. Collins, F., Lucy, A., Sharp, C. (1997), Oxidative desulphurisation of oils via hydrogen peroxide and heterpolynion catalysis. Journal of Molecular Catalysis, 117 397-403.
- 8. Duarte, F. A., Mello, P.A., Bizzi, C. A., Nunes, M.A., Moreira, E.M., Alencar, M. S. (...) Flores, E. M., (2011), Sulfur removal from hydrotreated petroleum fractions using ultrasound-assisted oxidative desulfurization process. Fuel, 90 2158-2164.
- 9. Feng, M. (2009), Review on recent patents in sulfur removal from liquid fuels by oxidative desulfurization (ODS) process. Recent Patents on Chemical Engineering,2010, 3, 30-37.
- 10. Gatan R., Barger P., Gembicki V., Cavanna A., Molinari D. (2004), Oxidative Desulfization: A New Technology for ULSD. Prepr. Pap.-Am. Chem. Soc., Div. Fuel Chem. 2004, 49(2), 579.
- 11. Liotta F., Han Y. (2003), Production of Ultra-Low Sulfur Fuels by Selective Hydroperoxide Oxidation. National Petrochemical & Refiners Association.
- 12. Stanislaus A., Marafi A., Rana, M. (2010), Recent advances in the science and technology of ultra low sulfur diesel (ULSD) production. Catalysis Today 153 1-68.
- Sundararaman, R., Ma, X., Song, C. (2010), Oxidative Desulfurization of Jet and Diesel Fuels Using Hydroperoxide Generated in Situ by Catalytic Air Oxidation. Ind. Eng. Chem. Res. 2010, 49, 5561– 5568.
- Wang, D., Qian, E.W., Amano, H., Okata, K., Ishihara, A., Kabe, T. (2003), Oxidative desulfurization of fuel oil Part I. Oxidation of dibenzothiophenesusing tert-butyl hydroperoxide. Applied Catalysis A: General 253, 91–99.
- 15. Zhang G., Yu F., Wang R. (2009), Research Advances In Oxidative Desulfurization Technologies For The Production Of Low Sulfur Fuel Oils. Petroleum & Coal 51(3) 196-207.
- 16. Zhou, X., Gai, H., Wang, J., Zhang, S., Yang J., Zhang, S. (2009), Oxidative desulfurization of fuel. Chinese Journal of Chemical Engineering, 17(2) 189-194.